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(54) Method of treating a subterranean formation

(57) A subterranean formation is treated with a particulate-laden fluid and a treatment chemical, whereby particulate flowback is reduced or prevented while also providing a controlled release of the treatment chemical within the formation. A fluid suspension including a mixture of a particulate, a tackifying compound and the

treatment chemical, is pumped into the formation and depositing therein within whereby the tackifying compound retards release of said treatment chemical and also retards movement of at least a portion of the particulate within the formation upon flow of fluids from the subterranean formation.

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Description

[0001] This invention relates to a method of treating a subterranean formation and, more particularly, to a method of providing delayed release of treatment chemicals into a subterranean formation in a substantially uniform manner and, optionally, for controlling particulate solids transport during the production of hydrocarbons from the formation.

[0002] Transport of particulate solids during the production of hydrocarbons from a subterranean formation is a continuing problem. The transported solids can erode or cause significant wear in the hydrocarbon production equipment used in the recovery process. The solids also can clog or plug the wellbore thereby limiting or completely stopping fluid production. Further, the transported particulates must be separated from the recovered hydrocarbons adding further expense to the processing.

[0003] The particulates which are available for transport may be present due to an unconsolidated nature of a subterranean formation and/or as a result of well treatments placing particulates in a wellbore or formation, such as, by gravel packing or propped fracturing.

[0004] In the treatment of subterranean formations, it is common to place particulate materials as a filter medium and/or a proppant in the near wellbore area and in fractures extending outwardly from the wellbore. In fracturing operations, proppant is carried into fractures created when hydraulic pressure is applied to these subterranean rock formations to a point where fractures are developed. Proppant suspended in a viscosified fracturing fluid is carried outwardly away from the wellbore within the fractures as they are created and extended with continued pumping. Upon release of pumping pressure, the proppant materials remain in the fractures holding the separated rock faces in an open position forming a channel for flow of formation fluids back to the wellbore.

[0005] Proppant flowback is the transport of proppants back into the wellbore with the production of formation fluids following fracturing. This undesirable result causes undue wear on production equipment, the need for separation of solids from the produced hydrocarbons and occasionally also decreases the efficiency of the fracturing operation since the proppant does not remain within the fracture and may limit the width or conductivity of the created flow channel. Proppant flowback often may be aggravated by what is described as "aggressive" flowback of the well after a stimulation treatment. Aggressive flowback generally entails flowback of the treatment fluid at a rate of from about 0.001 to about 0.1 barrels per minute (BPM) per perforation of the treatment fluids which were introduced into the subterranean formation. Such flowback rates accelerate or force closure of the formation upon the proppant introduced into the formation. The rapid flowrate can result in large quantities of the proppant flowing back into the wellbore before closure occurs or where inadequate bridging within the formation occurs. The rapid flowback is highly desirable for the operator as it returns a wellbore to production of hydrocarbons significantly sooner than would result from other techniques.

[0006] Currently, the primary means for addressing the proppant flowback problem is to employ resin-coated proppants or resin consolidation of the proppant which are not capable of use in aggressive flowback situations. Further, the cost of resin-coated proppant is high, and is therefore used only as a tail-in in the last five to twenty five percent of the proppant placement. Resin-coated proppant is not always effective since there is some difficulty in placing it uniformly within the fractures. Another means showing reasonable effectiveness has been to gradually release fracturing pressure once the fracturing operation has been completed so that fracture closure pressure acting against the proppant builds slowly allowing the proppant particles to stabilize before flowback of the fracturing fluid and the beginning of hydrocarbon production. Such slow return is undesirable, however, since it reduces the production from the wellbore until the treatment fluid is removed.

[0007] In unconsolidated formations, it is common to place a filtration bed of gravel in the near-wellbore area in order to present a physical barrier to the transport of unconsolidated formation fines with the production of hydrocarbons. Typically, such so-called "gravel packing operations" involve the pumping and placement of a quantity of gravel and/or sand having a mesh size between about 10 and 60 mesh on the U.S. Standard Sieve Series into the unconsolidated formation adjacent to the wellbore. It is sometimes also desirable to bind the gravel particles together in order to form a porous matrix through which formation fluids can pass while straining out and retaining the bulk of the unconsolidated sand and/or fines transported to the near wellbore area by the formation fluids. The gravel particles may constitute a resin-coated gravel which is either partially cured and subsequently completes curing or can be cured by an overflush of a chemical binding agent once the gravel is in place. It has also been known to add various hardenable binding agents or hardenable adhesives directly to an overflush of unconsolidated gravel in order to bind the particles together.

[0008] U. S. Patents 5,330,005, 5,439,055 and 5,501,275 disclose a method for overcoming the difficulties of resin coating proppants or gravel packs by the incorporation of a fibrous material in the fluid with which the particulates are introduced into the subterranean formation. The fibers generally have a length ranging upwardly from about 2 millimeters and a diameter of from about 6 to about 200 microns. Fibrillated fibers of smaller diameter also may be used.

The fibers are believed to act to bridge across constrictions and orifices in the proppant pack and form a mat or framework which holds the particulates in place thereby limiting particulate flowback. The fibers typically result in a 25 percent or greater loss in permeability of the proppant pack that is created in comparison to a pack without the fibers.

[0009] While this technique may function to limit some flowback, it fails to secure the particulates to one another in

the manner achieved by use of resin coated particulates. U.S. Patent 5,501,274 discloses a method for reducing proppant flowback by the incorporation of thermoplastic material in particulate, ribbon or flake form with the proppant. Upon deposition of the proppant and thermoplastic material in the formation, the thermoplastic material softens and causes particulates adjacent the material to adhere to the thermoplastic creating agglomerates. The agglomerates then bridge with the other agglomerates and other particulates to prevent flowback from the formation.

[0010] It would be desirable to provide a more permanent method which will bind greater numbers of particles of the particulate to one another whereby agglomerates may be formed which would further assist in preventing movement or flowback of particulates from a wellbore or formation without significantly reducing the permeability of the particulate pack during aggressive flowback of treatment fluids.

[0011] It is also desirable to provide a method by which a substantially uniform release of a treatment chemical such as a gel breaker, scale inhibitor, biocide, corrosion inhibitor, paraffin inhibitor or other treatment chemical may be effected within a proppant pack in a subterranean formation. It is also desirable to be able to control the rate of release of the treatment chemical within the subterranean formation.

[0012] We have now devised a method of treating a subterranean formation and uniformly delivering a controlled release of a treatment chemical to the formation.

[0013] In one aspect, the invention provides a method of treating a subterranean formation, which method comprises mixing with at least a portion of particulate in a particulate-containing fluid suspension a liquid or solution of a non-hardening tackifying compound whereby at least a portion of said particulate is at least partially coated by said compound; mixing with at least a portion of said particulate in said fluid suspension a treatment chemical whereby at least a portion of said treatment chemical is contacted by said tackifying compound and at least partially coated therewith, whereby the tackifying compound retards release of said treatment chemical in said fluid suspension; and depositing the tackifying compound-coated particulates and treatment chemical in the subterranean formation whereby, upon flowing back fluid from the formation, the tackifying compound-coated treatment chemical is subsequently released within the subterranean formation to treat at least a portion of the formation or fluids in contact therewith.

[0014] The method of the invention comprises providing a fluid suspension including a mixture of particulate material, a material comprising a liquid or solution of a tackifying compound, which coats at least a portion of the particulate upon admixture therewith, a treatment chemical which may be in particulate form or coated upon or in a substrate and, optionally, a hardenable resin, which coats or is coated upon at least a portion of the particulate, pumping the fluid suspension including the coated particulate and treatment chemical through the wellbore and depositing the mixture in the formation. Upon deposition of proppants having been coated with the tackifying compound and optionally the resin material mixture in the formation the coating causes particulate adjacent to the coated material as well as the dispersed treatment chemical particles to adhere to the coated material thereby creating proppant agglomerates which bridge against other particles in the formation to minimize initial particulate flowback and the hardenable resin, when present, subsequently consolidates the particulate.

[0015] The coated material is effective in inhibiting the flowback of particulate in a porous pack having a size ranging from about 2 to about 400 mesh in intimate admixture with the tackifying compound coated particulates.

[0016] The coated material is effective in consolidating particulate into the form of agglomerates in a formation as a result of a fracturing or gravel packing treatment performed on a subterranean formation during aggressive flowback of the treatment fluid.

[0017] In accordance with the present invention, a liquid or solution of a tackifying compound is incorporated in an intimate mixture with a particulate material such as conventional proppants or gravel packing materials together with an optional hardenable resin and introduced into a subterranean formation.

[0018] As used in this specification, the term "intimate mixture" will be understood to mean a substantially uniform dispersion of the components in the mixture. The term "simultaneous mixture" will be understood to mean a mixture of components that are blended together in the initial steps of the subterranean formation treatment process or the preparation for the performance of the treatment process.

[0019] The coated particulate or proppant material may comprise substantially any substrate material that does not undesirably chemically interact with other components used in treating the subterranean formation. The material may comprise sand, ceramics, glass, sintered bauxite, resin coated sand, resin beads, metal beads and the like. The coated material also may comprise an additional material that is admixed with a particulate and introduced into a subterranean formation to reduce particulate flowback. In this instance the additional substrate material may comprise glass, ceramic, carbon composites, natural or synthetic polymers or metal and the like in the form of fibers, flakes, ribbons, beads, shavings, platelets and the like. In this instance, the additional substrate material generally will be admixed with the particulate in an amount of from about 0.1 to about 5 percent by weight of the particulate.

[0020] Surprisingly, it has been found that the additional material also may comprise porous or non-porous substrates upon which a treatment chemical is either absorbed or coated or even particulates or agglomerates of particles of a desired solid treatment chemical which exhibits solubility in the formation fluids upon contact therewith. The additional material may or may not function as a proppant or gravel pack material in the subterranean formation, depending upon

the presence or absence of a substrate and its properties. The treatment chemical may comprise gel breakers, such as oxidizers, enzymes or hydrolyzable esters that are capable of producing a pH change in the fluid, scale inhibitors, biocides, corrosion inhibitors, paraffin inhibitors or substantially any other chemical which is soluble in the fluids in the formation at the temperature conditions within the formation within which it is placed. It has been found that the tackifying compound, upon at least partially coating the treatment chemical, retards the dissolution or absorption of the treatment chemical by the formation fluids. The treatment chemical is slowly released within the formation by contact with the fluids present in the formation. The tackifying compound changes the interfacial surface tension effects of the fluids in contact with the treatment chemicals to reduce wetting of the treatment chemicals by the formation fluids thereby reducing the dissolution rate of the chemicals. The presence of the tackifying compound on the particulate or substrate material causes the treatment chemical containing or coated particles to adhere to and remain dispersed within the coated particulate both during mixing, introduction into the formation and upon placement therein. The transported treatment chemicals are not subject to the gravity segregation or premature settling from the particulate material with which it is introduced. Thus, the treatment chemicals can be uniformly dispersed in a proppant pack or gravel pack without undesired segregation or settling to enable uniform release of the treatment chemical within the formation.

[0021] The tackifying compound comprises a liquid or a solution of a compound capable of forming at least a partial coating upon the substrate material with which it is admixed prior to or subsequent to placement in the subterranean formation. In some instances, the tackifying compound may be a solid at ambient surface conditions and upon initial admixing with the particulate and after heating upon entry into the wellbore for introduction into the subterranean formation become a melted liquid which at least partially coats a portion of the particulate. Compounds suitable for use as a tackifying compound comprise substantially any compound which when in liquid form or in a solvent solution will form a non-hardening coating, by themselves, upon the particulate which facilitates agglomeration and will increase the continuous critical resuspension velocity of the particulate when contacted by a stream of water as hereinafter described in Example I by at least about 30 percent over the particulate alone when present in a 0.5 percent by weight active material concentration. Preferably, the continuous critical resuspension velocity is increased by at least 50 percent over particulate alone. A particularly preferred group of tackifying compounds comprise polyamides which are liquids or in solvent solution at the temperature of the subterranean formation to be treated such that the polyamides are, by themselves, non-hardening when present on the particulates introduced into the subterranean formation. A particularly preferred product is a condensation reaction product comprised of commercially available polyacids and a polyamine. Such commercial products include compounds such as mixtures of C_{38} dibasic acids containing some trimer and higher oligomers and also small amounts of monomer acids which are reacted with polyamines. Other polyacids include trimer acids, synthetic acids produced from fatty acids, maleic anhydride and acrylic acid and the like. Such acid compounds are available from companies such as Witco, Union Carbide, Chemtall, and Emery Industries. The reaction products are available from, for example, Champion Chemicals, Inc. and Witco.

[0022] In general, the polyamides of the present invention are commercially produced in batchwise processing of polyacids predominately having two or more acid functionalities per molecule with a polyamine. As is well known in the manufacturing industry, the polyacids and polyfunctional amines are introduced into a reactor where, with agitation, the mildly exothermic formation of the amine salt occurs. After mixing, heat is applied to promote endothermic dehydration and formation of the polymer melt by polycondensation. The water of reaction is condensed and removed leaving the polyamide. The molecular weight and final properties of the polymer are controlled by choice and ratio of feedstock, heating rate, and judicious use of monofunctional acids and amines to terminate chain propagation. Generally an excess of polyamine is present to prevent runaway chain propagation. Unreacted amines can be removed by distillation, if desired. Often a solvent, such as an alcohol, is admixed with the final condensation reaction product to produce a liquid solution that can readily be handled. The condensation reaction generally is accomplished at a temperature of from about 225°F to about 450°F under a nitrogen sweep to remove the condensed water from the reaction. The polyamines can comprise, for example, ethylenediamine, diethylenetriamine, triethylene tetraamine, amino ethyl piperazine and the like.

[0023] The polyamides can be converted to quaternary compounds by reaction with methylene chloride, dimethyl sulfate, benzylchloride, diethyl sulfate and the like. Typically the quaternization reaction would be effected at a temperature of from about 100 to about 200°F over a period of from about 4 to 6 hours.

[0024] The quaternization reaction may be employed to improve the chemical compatibility of the tackifying compound with the other chemicals utilized in the treatment fluids. Quaternization of the tackifying compound can reduce effects upon breakers in the fluids and reduce or minimize the buffer effects of the compounds when present in various fluids.

[0025] Additional compounds which may be utilized as tackifying compounds include liquids and solutions of, for example, polyesters, polyethers and polycarbonates, polycarbonates, styrene-butadiene latices, natural or synthetic resins such as shellac and the like.

[0026] The tackifying compound is admixed with the particulate and the treatment chemical particles in an amount of from about 0.1 to about 3.0 percent active material by weight of the coated particulate. It is to be understood that

larger quantiles may be used, however, the larger quantiles generally do not significantly increase performance and could undesirably reduce the permeability of the particulate pack. Preferably, the tackifying compound is admixed with the particulate and treatment chemical particles introduced into the subterranean formation in an amount of from about 0.25 to about 2.0 percent by weight of the coated particulate.

[0027] When the tackifying compound is utilized with another material that is to be admixed with the particulate and which is to be at least partially coated with the tackifying compound, such as glass fibers or the like, the compound is present in an amount of from about 10 to about 250 percent active material by weight of the glass fibers or other added material and generally from about 0.1 to about 3 percent active material by weight of the quantity of particulate with which the coated material is intimately admixed. Preferably the tackifying compound is present in an amount of from about 50 to about 150 percent of the material which is to be at least partially coated with the tackifying compound and then added to the particulate. At least a portion of the tackifying compound introduced with the additional material will contact and coat at least a portion of the particulate with which it is admixed.

[0028] The hardenable resin, when present, comprises an epoxy or phenolic resin or other compound capable of being at least partially coated upon a particulate substrate and then cured to a higher degree of polymerization. Examples of such resins include phenol-aldehyde resins of both the resole and novolac type, urea-aldehyde resins, melamine-aldehyde resins, epoxy resins, furfuryl alcohol resins and the like. The curing may result from heating the resin to a higher temperature such as can occur with the resole resins or by the addition of a catalyst or crosslinker to the resin which initiates polymerization. Admixtures of resins such as the resole and novolac resins may be utilized wherein sufficient resole resin is incorporated to initiate polymerization in the novolac resin. Various resins are described in for example U.S. Patents 5,420,174; 5,218,038; 5,425,994 and 4,888,240 the entire disclosures of which are incorporated herein by reference thereto. Particularly preferred resins include epoxy resins such as "EPON 828" epoxy resin from Shell Chemical Company, Houston, Texas. Phenolic resins such as "Resin 1866" from Acme Resin Corporation, Borden Division, Forrest Park, Illinois, furan resins such as "ARS-1500" resin from Advanced Resin Systems, Des Plaines, Illinois and novolac Resins such as "Bakelite 9282 FP" resin also available from Advanced Resin Systems.

[0029] The resin is admixed with the particulate in an amount of from about 0.01 to about 5.0 percent by weight of the particulate. Preferably, the resin is admixed with the particulate in an amount of from about 0.05 to about 1.0 percent by weight of the particulate. Curing agents, catalysts or crosslinkers selected from those well known in the art may be utilized with the resin to harden the resin and form a consolidated matrix of particulate.

[0030] The liquid or solution of tackifying compound interacts mechanically with the particles of particulate introduced into the subterranean formation to limit or prevent the flowback of particulates to the wellbore during initial flowback. When the hardenable resin is present, the tackifying compound substantially limits flowback prior to hardening and consolidation of the particulates by the hardenable resin.

The tackifying compound causes the treatment chemical particles admixed with the coated particulates to adhere to the coated particles and to remain uniformly dispersed within the portion of the coated particulate to which it is added.

[0031] In one embodiment, the tackifying compound, when comprised of polyamides that contain reactive sites such as amine groups, may be admixed and contacted with a material that has multi-functional reactive sites which are capable of reacting with the reactive sites on the tackifying compound to form a hard reaction product which consolidates the agglomerates formed by the tackifying compound. A "hard reaction product" as used herein means that the reaction of the tackifying compound with the multifunctional material will result in a substantially nonflowable reaction product that exhibits a higher compressive strength in a consolidated agglomerate than the tackifying compound alone with the particulates. One means of evaluating the consolidated agglomerate to determine whether an increase in compressive strength has occurred is through testing with a penetrometer. Samples may be prepared comprising particulate coated with the tackifying compound, multifunctional material and an admixture as described herein and penetrometer readings can be made using equipment such as a PWG Penetrometer from Precision Scientific Company, Chicago, Illinois. Comparison of the penetrometer readings readily demonstrates the change that has occurred as a result of the reaction. In this instance, the tackifying compound also functions as the hardenable resin. The material having multi-functional reactive sites include compounds such as aldehydes such as formaldehyde, dialdehydes such as glutaraldehyde, hemiacetals or aldehyde releasing compounds, diacid halides, dihalides such as dichlorides and dibromides, polyacid anhydrides such as citric acid anhydride, epoxides and the like. Preferred compounds for use with polyamides containing reactive sites comprise furfuraldehyde, glutaraldehyde or aldehyde condensates and the like. The multi-functional compound is admixed with the tackifying compound in an amount of from about 0.01 to about 50 percent by weight of the tackifying compound to effect formation of the reaction product. Preferably, the compound is present in an amount of from about 0.5 to about 1 percent by weight of the tackifying compound.

[0032] The liquid or solution of tackifying compound and hardenable resin generally are incorporated with the particulate in any of the conventional fracturing or gravel packing fluids comprised of an aqueous fluid, an aqueous foam, a hydrocarbon fluid or an emulsion, a viscosifying agent and any of the various known breakers, buffers, surfactants, clay stabilizers or the like.

[0033] Generally the tackifying compound and hardenable resin may be incorporated into fluids having a pH in the

range of from about 3 to about 12 for introduction into a subterranean formation. The compounds are useful in reducing particulate movement within the formation at temperatures from about ambient to in excess of 300°F. It is to be understood that not every hardenable resin or tackifying compound will be useful over the entire pH or temperature range but every compound is useful over at least some portion of the range and individuals can readily determine the useful operating range for various products utilizing well known tests and without undue experimentation.

[0034] The liquid or solution of tackifying compound and the hardenable resin generally are incorporated with the particulate as a simultaneous mixture by introduction into the fracturing or gravel packing fluid along with the particulate. The treatment chemical may be introduced in a similar manner and may be at least partially coated by the tackifying compound or may adhere to the particulate which has been at least partially coated with the tackifying compound. Fracturing fluid slurries are introduced into the subterranean formation at a rate and pressure sufficient to create at least one fracture in the formation into which particulate then is introduced to prop the created fracture open to facilitate hydrocarbon production. Gravel packing treatments generally are performed at lower rates and pressures whereby the fluid can be introduced into a formation to create a controlled particle size pack surrounding a screen positioned in the wellbore where fracturing of the formation may or may not occur. The particulate pack surrounding the wellbore then functions to prevent fines or formation particulate migration into the wellbore with the production of hydrocarbons from the subterranean formation. The treatment chemical then is dissolved by the fluids present in the formation to provide the desired treatment. The dissolution may be effected with either the natural formation fluids or a fluid that may be introduced into the formation specifically to dissolve the treatment chemical.

[0035] The gravel packing treatment also may be performed without a screen in the wellbore. In such a screenless completion, the fluid generally is introduced into the wellbore to fill the perforations and wellbore to a level above the perforations and permitted to consolidate. The consolidated pack can then be drilled or reamed out to reopen the bore while providing a consolidated pack to screen fines and formation particulate from migrating into the wellbore. When the treatment chemical comprises a breaker, uniform dispersion within the particulate pack can result in better clean-up of viscosifying agents from the gravel pack and higher pack permeability and less formation damage from the filter cake.

[0036] The tackifying compound may be introduced into the fluid before, after or simultaneously with introduction of the particulate into the fluid. The liquid or solution may be incorporated with the entire quantity of particulate introduced into the subterranean formation or it may be introduced with only a portion of the particulate, such as in the final stages of the treatment to place the intimate mixture in the formation in the vicinity of the wellbore. For example, the tackifying compound may be added to only the final 20 to 30 percent of the particulate laden fluid introduced into the formation and the hardenable resin may be added to only the last 10 to 20 percent of the particulate laden fluid. In this instance, the intimate mixture will form a tail-in to the treatment which upon interaction within the formation with the particulate will cause the particles to bridge on the agglomerates formed therein and prevent movement of the particles into the wellbore with any produced fluids. The tackifying compound and hardenable resin may be introduced into the blender or into any flowline in which they will contact the material to be at least partially coated by the compounds. The compounds may be introduced with metering pumps or the like prior to entry of the treatment fluid into the subterranean formation. The treatment chemicals generally will be introduced into those portions of the particulate that are coated with the tackifying compound unless the treatment chemical is itself at least partially coated with the tackifying compound. In this instance, the treatment chemical may be introduced with any of the particulate introduced into the subterranean formation.

[0037] In an alternate embodiment, the particulate may be premixed with either the tackifying compound or the hardenable resin prior to admixing with a treatment fluid and the other constituents for use in a subterranean formation. In some instances, resin precoated particulates may be utilized and the tackifying compound then would be added during performance of the subterranean formation treatment. Depending upon the type of resin coating employed, a catalyst then would be added to the treatment fluid or introduced in a flush fluid or the like.

[0038] Surprisingly, it has been found that use of the method of the present invention can produce high permeability tunnels extending from wellbore perforations back into proppant packed fractures created in the subterranean formation which then may be consolidated. Control of the flowback rate of the treatment or formation fluids from the wellbore can be used to provide a controlled erosion of the treated particulate immediately adjacent a perforation in the wellbore. The flowback rate is controlled so as to provide a level above the initial critical resuspension velocity of the tackifying compound but generally is maintained below the continuous critical resuspension velocity. This results in controlled production of particulate from the formation. The erosion surprisingly has been found to be very uniform in nature and to create a tunnel into the particulate in the formation generally corresponding to the size and shape of the perforation in the wellbore. After the tunnel is formed, the hardenable resin consolidates the remaining particulate to provide a high permeability passage or tunnel from the formation to the wellbore.

[0039] To further illustrate the present invention and not by way of limitation, the following examples are provided.

EXAMPLE I

[0040] The evaluation of a liquid or solution of a compound for use as a tackifying compound is accomplished by the following test. A critical resuspension velocity is first determined for the material upon which the tackifying compound is to be coated. The apparatus comprises a 1/2" glass tee which is connected to an inlet source of water and an outlet disposal line is blocked to fluid flow. A water slurry of particulate is aspirated into the tee through the inlet and collected within a lower portion of said tee by filtration against a screen. When the lower portion of the tee is full, the vacuum source is removed and a plug is used to seal the end of the lower portion of the tee. The flow channel from inlet to outlet then is swabbed clean and a volumetrically controlled pump, such as a "MOYNO" pump, is connected to the inlet and a controlled flow of water is initiated. The velocity of the fluid is slowly increased through the inlet until the first particle of particulate material is picked up by the flowing water stream. This determines the baseline for the starting of the resuspension velocity. The flow rate then is further increased until the removal of particles becomes continuous. This determines the baseline for the continuous resuspension velocity. The test then is terminated and the apparatus is refilled with particulate having a coating corresponding to about 0.5 percent active material by weight of the particulate applied thereto. Similar trends generally are seen in the results when the concentrations tested are from about 0.1 to about 3 percent, however, the 0.5 percent level which is within the preferred application range is preferred for standardization of the procedure. The test is repeated to determine the starting point of particulate removal and the velocity at which removal becomes continuous. The percent of velocity increase (or decrease) then is determined based upon the initial or continuous baseline value. The results of several tests employing the preferred polyamide of the present invention, and conventional epoxy and phenolic resins known for use in consolidation treatments in subterranean formations with 12/20 and 20/40 mesh sand are set forth below in Table I.

TABLE I

Test No.	Particulate Size	Coating Agent, % V/Wt Particulate	Percent Of Velocity Change At Starting of Sand Particle Transport		Continuous Sand Transport
1	20/40/mesh sand	None	0		
2	20/40 mesh sand	1/2 percent polyamide	192		222
3	20/40 mesh sand	1 percent polyamide	271		391
4	20/40 mesh sand	1/2 percent phenolic	-0.5		6.5
5	20/40 mesh sand	1 percent phenolic	-9		-6.8
6	20/40 mesh sand	1/2 percent epoxy	-9		-1.2
7	20/40 mesh sand	1 percent epoxy	5.2		12.2
8	12/20 mesh sand	1/2 percent polyamide	228		173
9	12/20 mesh sand	1 percent polyamide	367		242
10	12/20 mesh sand	1/2 percent phenolic	42		22
11	12/20 mesh sand	1 percent phenolic	42		13
12	12/20 mesh sand	1/2 percent epoxy	48		30
13	12/20 mesh sand	1 percent epoxy	38		15

[0041] The data clearly illustrates the substantial increase in the critical resuspension velocity of a particulate coated with the tackifying compound in comparison to other known formation consolidation agents which require hardening to be effective.

[0042] The test results clearly demonstrate the beneficial results achieved by practice of the method of the present invention with respect to proppant production from a simulated formation.

EXAMPLE II

[0043] The stabilization properties of the method of the present invention are determined by comparison to untreated sand and sand including a tackifying compound. The flowback velocity is measured in an American Petroleum Institute approved simulated fracture flow cell. The cell contains Ohio sandstone cores having a proppant bed size of about 1.5 inches in height, about 7 inches in length and about 0.25 inches in width between the cores. The bed is initially pre-packed with 20/40 mesh sand by introducing the sand into the cell in an aqueous slurry or a gelled fluid containing 40 pounds of guar per 1000 gallons of aqueous fluid. The cell is fitted with a 0.3 inch hole at one end to simulate a perforation. The hole is visible through a sight glass so that proppant production through the hole can be visually

determined.

[0044] The cell then was cleaned and packed with another proppant pack for testing. The tested materials are set forth in Table II, below.

TABLE II

SAMPLE	PACKING FLUID	ADDITIVES TO SAND, % BY WT. SAND	FLOW RATE, ml/min AT WHICH FAILURE OCCURS
1	water	None	84
2	gel	None	90
3	gel	1% by wt polyamide	180
4	gel	2% by wt polyamide	384
5	gel	1% by wt polyamide and 1% out Bakelite 9282 FP resin	>3000 ¹
6	gel	1% by wt polyamide and 1% by wt Bakelite 9282 FP resin	>2600 ²

1. pack heated at 250°F for 72 hours before testing, no sand production during test
2. pack heated at 180°F for 4 hours before testing no sand production during test

EXAMPLE III

[0045] The controlled release properties of the method of the present invention are determined by comparison to breaker solutions, untreated substrates containing breakers and substrates containing breaker including a tackifying compound.

[0046] The breaker utilized comprised sodium persulfate. The solution was prepared by dissolving 3 grams of sodium persulfate in 100 ml of deionized water. The particular substrates utilized comprised diatomaceous earth and amorphous silica. The diatomaceous earth substrate was prepared by dissolving 5 grams of sodium persulfate in 10 ml of deionized water to which was added 10 grams of diatomaceous earth. The sample then was dried for 24 hours in a 140°F vacuum oven. The sample material has a concentration of 0.5 gram sodium persulfate per gram of diatomaceous earth. The amorphous silica substrate was prepared by dissolving 5 grams of sodium persulfate in 10 ml of deionized water to which was added 5 grams of amorphous silica. The sample then is dried for 24 hours in a 140°F vacuum oven. The sample material has a concentration of 1 gram sodium persulfate per gram of amorphous silica.

[0047] The samples are admixed with a quantity of a crosslinked hydroxypropylguar containing fluid. The gelled fluid is prepared by hydrating hydroxypropylguar in tap water in an amount of 25 pounds per 1000 gallons of fluid. A liquid borate containing crosslinker such as described in U.S. Patent 5,827,804 issued October 27, 1998, the entire disclosure of which is incorporated herein by reference, then was admixed with the gelled fluid in an amount of 2 gallons per 1000 gallons of fluid. The crosslinked fluid then is admixed with a quantity of 20-40 mesh sand, tackifying compound and breaker or substrate loaded breaker in a concentration of 2 lbs. sodium persulfate per 1000 gallons of fluid. The tack-

ifying compound was admixed with the sand and substrate prior to admixture with the crosslinked gel resulting in a partial coating of the substrate with the tackifying compound. The tackifying compound is present in an amount of 1.2 percent by weight of the sand present. Each sample is placed in a beaker and heated to 150°F in a hot water bath. At designated intervals, the viscosity is measured on a Model 35 FANN™ Viscometer. The results of the tests are set forth in the Table III, below.

TABLE III

Sample No:	Breaker	pH	Tackifying Compound Present	Viscosity, cp			
				0.5hr	1hr	2hr	3.5hr
1	LS	8.47	No	C	C	1.5	1
2	LS	8.40	Yes	C	C	5	2.5
3	DE	8.45	No	C	C	1.5	1
4	AS	8.47	No	C	C	3	1.5
5	DE	8.48	Yes	C	C	9	3
6	AS	8.43	Yes	C	C	80	5
LS : liquid breaker solution DE : diatomaceous earth substrate with breaker AS : amorphous silica substrate with breaker C : fully crosslinked fluid							

[0048] The results clearly demonstrate the tackifying compound delayed the release of the breaker from the substrate material.

[0049] While the present invention has been described with regard to that which is currently considered to comprise the preferred embodiments of the invention, other embodiments have been suggested and still other embodiments will occur to those individuals skilled in the art upon receiving the foregoing specification. It is intended that all such embodiments shall be included within the scope of the present invention as defined by the claims appended hereto.

Claims

1. A method of treating a subterranean formation, which method comprises mixing with at least a portion of particulate in a particulate-containing fluid suspension a liquid or solution of a non-hardening tackifying compound whereby at least a portion of said particulate is at least partially coated by said compound; mixing with at least a portion of said particulate in said fluid suspension a treatment chemical whereby at least a portion of said treatment chemical is contacted by said tackifying compound and at least partially coated therewith, whereby the tackifying compound retards release of said treatment chemical in said fluid suspension; and depositing the tackifying compound-coated particulates and treatment chemical in the subterranean formation whereby, upon flowing back fluid from the formation, the tackifying compound-coated treatment chemical is subsequently released within the subterranean formation to treat at least a portion of the formation or fluids in contact therewith.
2. A method according to claim 1, wherein said particulate-containing fluid suspension is formed by introducing a treatment fluid into said subterranean formation; admixing with at least a portion of said fluid, a particulate which is to be introduced into and deposited within a fracture; and wherein said tackifying compound comprises a polyamide and said at least a portion of said particulate at least partially coated by said compound is such that the critical resuspension velocity of said at least partially coated particulate is increased by at least 30 percent when tested at a level of 0.5% active material by weight over said particulate alone with water.
3. A method according to claim 2, wherein said coated particulate has a critical resuspension velocity in excess of 100 percent over said particulate alone.
4. A method according to claim 2 or 3, wherein said polyamide comprises predominantly a condensation reaction product of a dimmer acid containing some trimer and higher oligomers and some monomer acids with a polyamine.